

Figure 1: Test stand for combustion catalysts

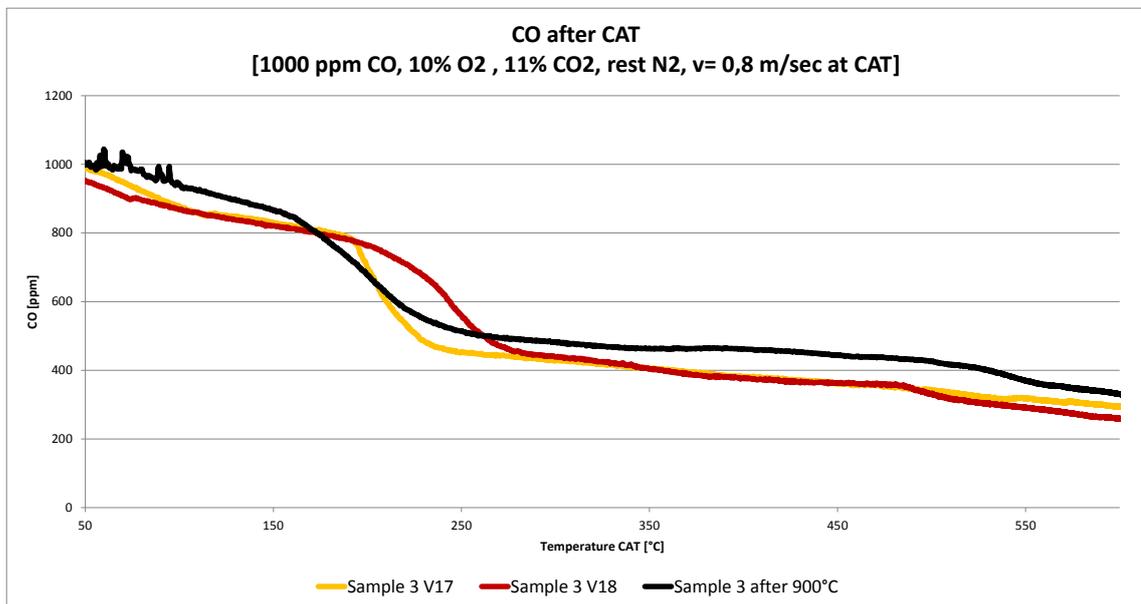


Figure 2: Reactivity of catalyst after thermal treatment

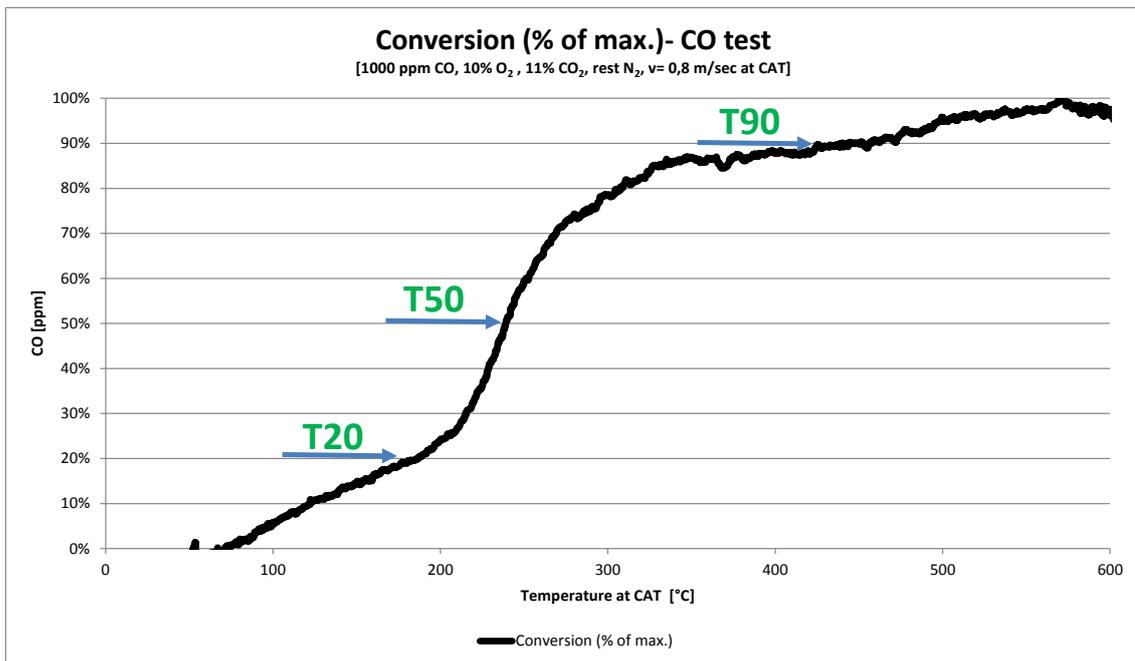


Figure 3: Conversion rate of CO on the catalyst

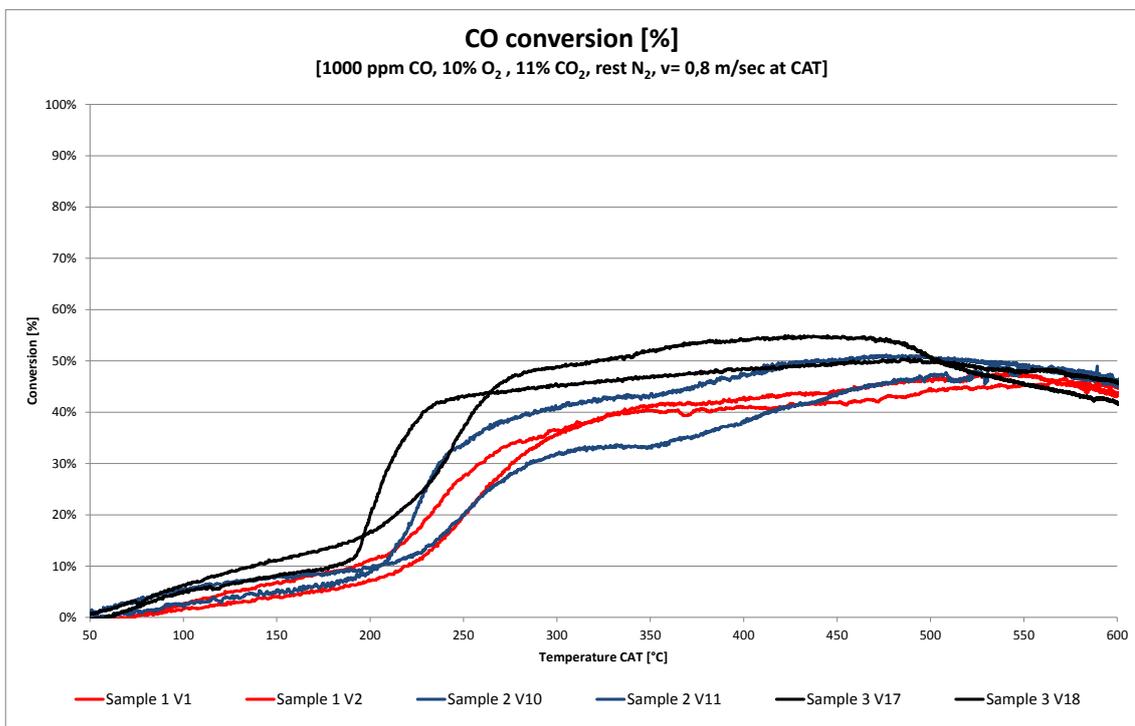


Figure 4: CO conversion rate.

Table 1: Characteristic temperatures for CO conversion

	Sample 1 average (n=3)	Sample 2 average (n=2)	Sample 3 average (n=2)	Total average (n=7)
T20	201°C	205°C	165°C	190°C
T50	249°C	246°C	220°C	238°C
T90	421°C	418°C	305°C	381°C

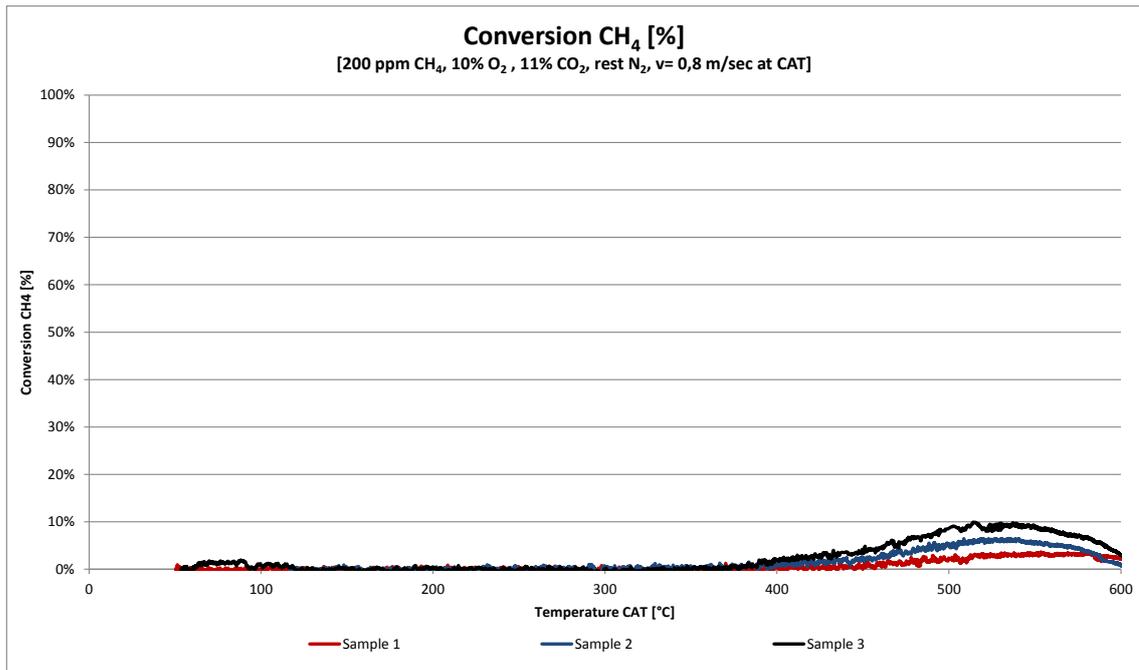


Figure 5: Conversion of methane depending on catalyst temperature

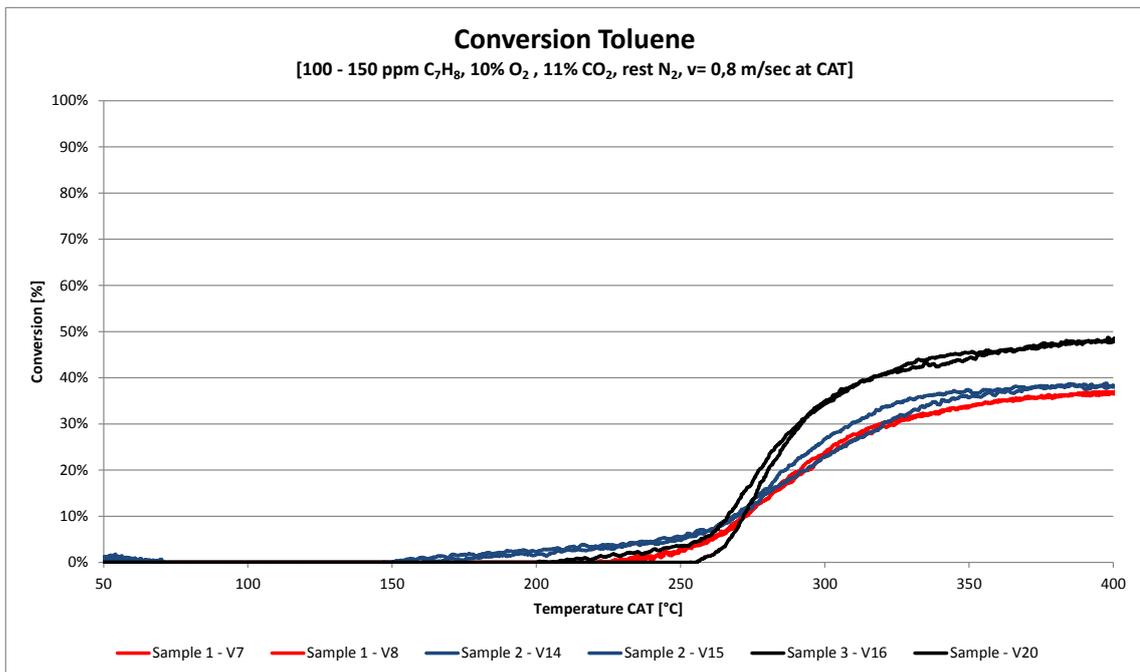


Figure 6: Conversion of toluene depending on catalyst temperature

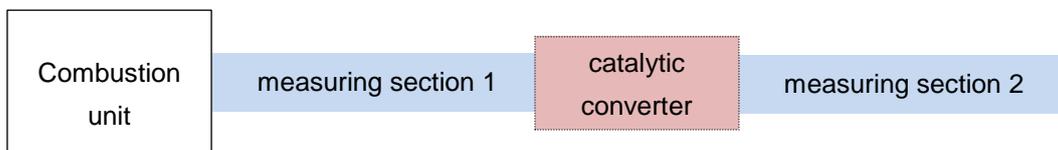


Figure 7: Parallel measuring up- and downstream of the catalytic converter

Equation 1: Conversion rate calculation

$$\text{conversion rate (\%)} = \frac{m_{\text{upstream CAT}} - m_{\text{downstream CAT}}}{m_{\text{upstream CAT}}} \times 100$$

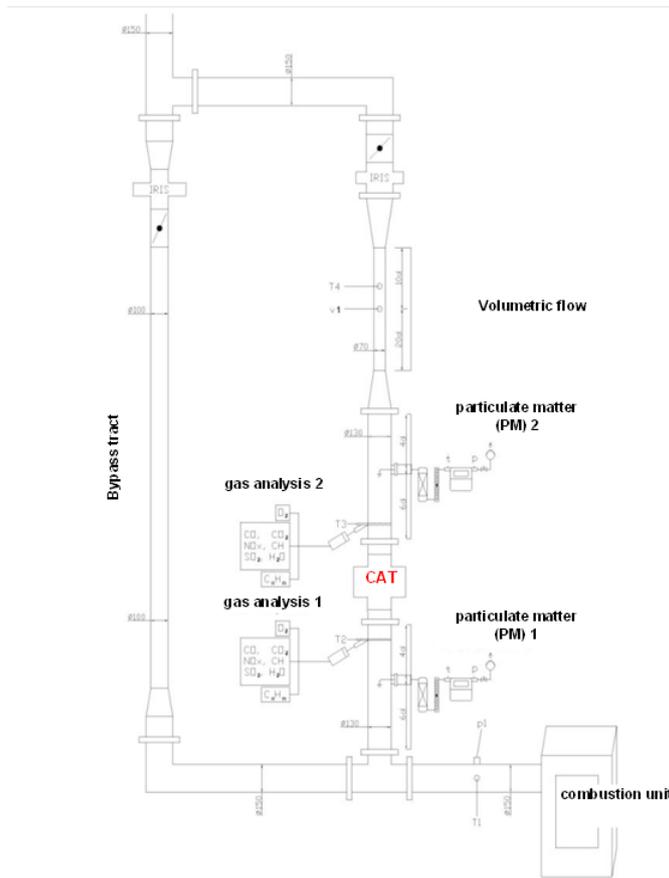


Figure 8: Setup of test stand for catalyst testing under real combustion gas conditions

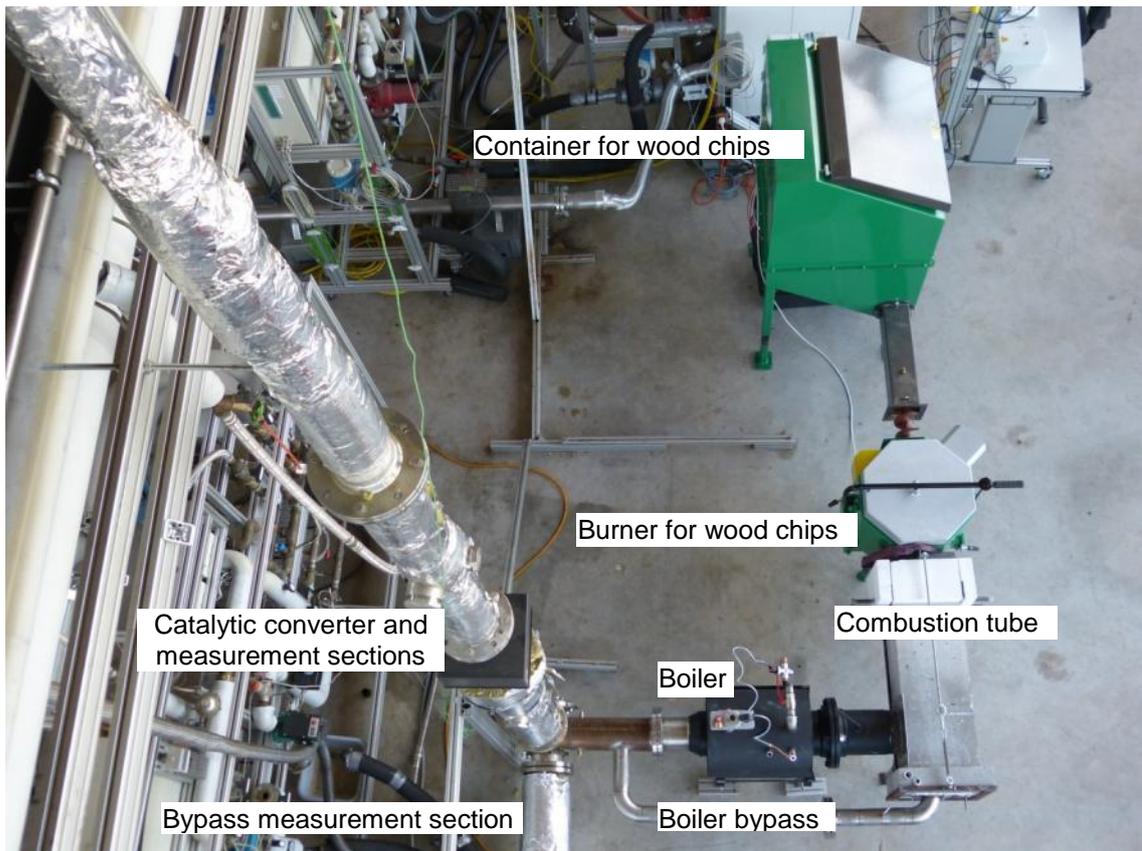


Figure 9: Setup of test stand

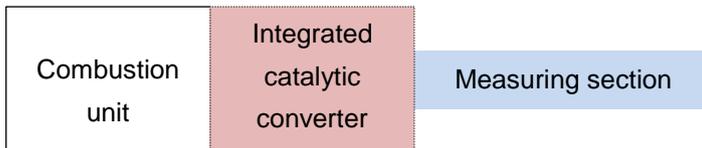


Figure 10: Measuring downstream of the catalytic converter

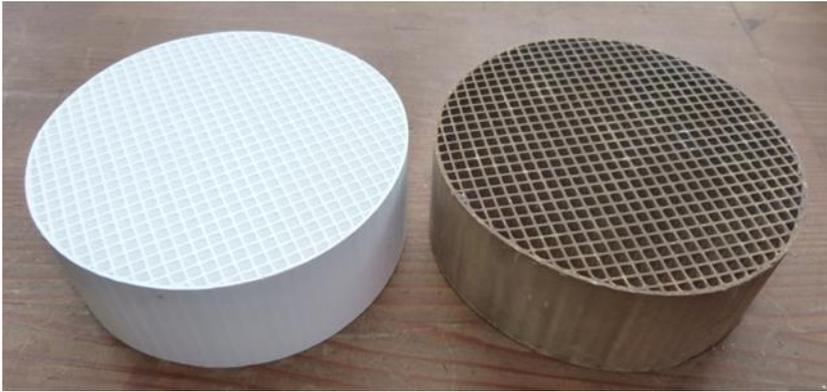


Figure 11: Unused honeycomb mullite ceramic without (left) and with (right) catalytic coating.

Equation 2: Variance with catalyst-dummy

$$s_1^2 = \frac{\sum_{(1)}(x - \bar{x}_1)^2}{n_1 - 1}$$

s_1^2 : estimated variance of the tests conducted with catalyst – dummy

\bar{x}_1 : arithmetic mean of the tests conducted with catalyst – dummy

n_1 : number of repetitions of the tests conducted with catalyst – dummy

Equation 3: Variance with catalyst

$$s_2^2 = \frac{\sum_{(2)}(x - \bar{x}_2)^2}{n_2 - 1}$$

s_2^2 : estimated variance of the tests conducted with catalyst

\bar{x}_2 : arithmetic mean of the tests conducted with catalyst

n_2 : number of repetitions of the tests conducted with catalyst

Equation 4: Variance of the difference

assumption: Same variance for repetitions with catalyst-dummy and with catalyst

$$s^2 = \frac{\sum_{(1)}(x - \bar{x}_1)^2 + \sum_{(2)}(x - \bar{x}_2)^2}{n_2 + n_1 - 2}$$

s^2 : estimated variance of the difference of the arithmetic means

Equation 5: Standard error of the difference

$$SE_{(\bar{x}_1 - \bar{x}_2)} = \sqrt{s^2 \cdot \left(\frac{1}{n_1} + \frac{1}{n_2}\right)}$$

$SE_{(\bar{x}_1 - \bar{x}_2)}$: standard error of the difference of the arithmetic means

Equation 6: Confidence limits

$$\bar{x}_1 - \bar{x}_2 \pm t_{v,\alpha} \cdot SE_{(\bar{x}_1 - \bar{x}_2)}$$

t : t distribution

v : degree of freedom

α : level of significance, corresponding level of confidence = $1 - \alpha$

Equation 7: Significant conversion

$$\text{significant conversion} = \bar{x}_1 - \bar{x}_2 - t_{v,\alpha} \cdot SE_{(\bar{x}_1 - \bar{x}_2)}$$

Equation 8: Significant conversion rate

$$\text{significant conversion rate} = \frac{\text{significant conversion}}{\bar{x}_1}$$

Table 2: Improvement in emissions and energy efficiency by primary measures

Parameter	Appliance No			
	1	2	3	5
	Relative improvement from initial state			
CO	- 74 %	- 63 %	- 44 %	- 56 %
VOC	- 72 %	- 40 %	- 47 %	- 78 %
η	+ 59 %	+ 7 %	\pm 0 %	+ 34 %

Round shape; ceramic **Rectangular shape; ceramic** **Round shape; metallic**



Figure 12: Honey comb catalysts of different shape and carrier materials

Table 3: Overview on type testing results (emissions based on 13 % O₂)

Combustion system	Hapero	Rika	Stuv 16-78	Stuv 30.3-IN	Staffieri
Testing institute:	TU-Wien	TGM	SGS	SGS	TU-Wien
CO [mg/Nm ³]	836	209	117	391	n.a. ¹
OGC [mg/Nm ³]	8	45	32	78	n.a. ¹
PM [mg/Nm ³]	63	19	27	29	n.a. ¹
η [%]	79	75	79	79	n.a. ¹

Table 4: Target values at the beginning of the project (emissions based on 13 % O₂)

Combustion system	Hapero	Rika	Stuv 16-78	Stuv 30.3-IN	Staffieri
CO [mg/Nm ³]	200	200	500	400	1000
PM [mg/Nm ³]	25	20	30	25	40

¹ Type testing results are coming up soon